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CLOSED CYCLE BRAYTON PROPULSION SYSTEM
WITH DIRECT HEAT TRANSFER

TO ALL WHOM IT MAY CONCERN

BE IT KNOWN THAT PAUL M. DUNN, citizen of the United States of America, employee of the United States Government and resident of Wakefield, County of Washington, State of Rhode Island has invented certain new and useful improvements entitled as set forth above of which the following is a specification:

Michael J. McGowan
Reg. No. 31042
Naval Undersea Warfare Center
Division, Newport
Newport, Rhode Island 02841-5047
TEL: 401-841-4736
FAX: 401-841-1231



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2 CLOSED CYCLE BRAYTON PROPULSION SYSTEM
3 WITH DIRECT HEAT TRANSFER

4
5 This patent application is copending with the related
6 applications by the same inventor filed on the same date as
7 subject patent entitled Closed Brayton Cycle Direct Contact

8 a ~~0183~~ Reactor/Storage Tank with Chemical Scrubber, identified as ^{Serial} Navy
9 a ~~No. 07/926,090, filed 7 August 1992~~
Case No. ~~72910~~, Closed Brayton Cycle Direct Contact

10 a ~~0184~~ Reactor/Storage Tank with ~~an~~ Afterburner, identified as ^{Serial No.} Navy Case

11 a ~~07/926,200, filed 7 August 1992~~ Semiclosed Brayton Cycle
Case No. ~~72939~~, Closed Cycle Brayton Power System with Direct Heat

12 a ~~0185~~ Transfer, identified as Navy Case No. ~~73348~~, and Semiclosed
Power System

13 a ~~0186~~ Brayton Cycle with Direct Combustion Heat Transfer, identified as
Serial No. ~~07/926,199, filed August 7, 1992~~
Navy Case No. ~~73825~~.

15
16 STATEMENT OF GOVERNMENT INTEREST

17 The invention described herein may be manufactured and used
18 by or for the Government of the United States of America for
19 Governmental purposes without the payment of any royalties
20 thereon or therefor.

21
22 BACKGROUND OF THE INVENTION

23 (1) Field of the Invention

24 The invention relates generally to non-air breathing power
25 systems and, in particular, to a closed Brayton cycle propulsion
26 system using direct heat transfer.

(2) Description of the Prior Art

Torpedoes and other underwater vehicles use propulsion systems having turbines powered by the reaction of an oxidant with a metal fuel in a liquid state, hereinafter referred to as liquid metal fuel, as a heat source. Lithium or another alkali metal is commonly used as liquid metal fuel with sulphur hexafluoride, SF₆, as the oxidant. A chlorofluorocarbon, such as C₂F₃Cl₃, known in the art as Freon-13, can also be used as the oxidant. Another possible liquid metal fuel is an aluminum-magnesium alloy with O₂ as the oxidant. Chlorofluorocarbons cannot be used with an aluminum-magnesium fuel because AlCl, one of the products of the reaction, is gaseous at operating temperatures.

Current underwater propulsion systems are typically closed Rankine cycle power systems utilizing lithium as a liquid metal fuel, a chlorofluorocarbon as an oxidant, and water as a working fluid. In a typical Rankine system, the working fluid is compressed, heated until vaporization, and then expanded through a turbine to produce power. Upon exiting the turbine, the low pressure vapor is condensed to a liquid, and the cycle is repeated. The working fluid is heated as it passes through heat transfer tubes that are wrapped to form a cylindrical annulus within the system's heat exchanger. Liquid metal fuel is contained in the center of the cylinder in order to heat the working fluid being carried by the heat transfer tubes. The working fluid, water, and the liquid metal fuel, lithium, react

1 chemically with one another. A leak in the heat transfer tubes
2 causes a violent reaction which generates a significant amount of
3 heat and gas causing the heat exchanger and the underwater device
4 to fail. Furthermore, should a leak occur in a land-based
5 system, a toxic cloud of LiOH will be released into the
6 environment. Other problems associated with the Rankine cycle
7 include noise generation during the phase change of the working
8 fluid, severe stress of the oxidant's injectors due to high
9 reaction zone temperatures, and slow start-up time.

10 An alternative to the closed cycle Rankine system is the
11 closed Brayton cycle system. In a Brayton cycle, there is no
12 phase change and accordingly, no noise associated therewith. The
13 Brayton cycle is also more efficient than the Rankine cycle
14 despite the fact that more energy is required to compress a gas
15 than to pump an equivalent mass of liquid. Prior art Brayton
16 cycle systems cannot be used in underwater systems because the
17 components of the closed Brayton cycle, principally the
18 conventional Brayton heat exchanger, are too large to be used in
19 the restricted space available in underwater vehicles.

20 A compact heat exchanger can be made by increasing gas
21 velocity to achieve higher heat transfer coefficients; however,
22 this results in greater heat exchanger pressure drop. This
23 method is used successfully in the Rankine cycle since pump power
24 is a small fraction of gross power (1/50) and pump losses are
25 small by comparison. Accordingly, there is no significant
26 reduction in cycle efficiency. In the Brayton cycle, however,

1 compressor power is typically a large part of the gross power
2 (1/2); therefore, small increases in gas velocity and heater
3 pressure drop reduce the Brayton cycle efficiency below that of
4 the Rankine cycle.

5

6 SUMMARY OF THE INVENTION

7 Accordingly, it is an object of the present invention to
8 provide a closed Brayton cycle power system for use in an
9 underwater vehicle propulsion system.

10 Another object of the present invention is to provide a
11 closed Brayton cycle power system that utilizes a compact heat
12 exchanger with low pressure drop.

13 Another object of the present invention is to provide a
14 closed Brayton cycle power system that will propel an underwater
15 vehicle for longer periods of time.

16 In accordance with the present invention, a liquid metal
17 fueled Brayton cycle power system is used to power an underwater
18 device. A compressor is provided to compress the working gas.
19 The compressed working gas is then preheated in a regenerator and
20 passed to a reactor/storage tank. Liquid metal fuel is stored
21 within the reactor/storage tank. An oxidant is injected into the
22 reactor/storage tank to react with the liquid metal fuel and
23 thereby generate heat. The compressed working gas is bubbled
24 through the liquid metal fuel/oxidant mixture and heated by
25 direct contact. A turbine is provided for expanding the working
26 gas and withdrawing power from the system. The working gas is
27 cooled and recirculated.

1 BRIEF DESCRIPTION OF THE DRAWINGS

2 Other objects, features and advantages of the present
3 invention will become apparent upon reference to the following
4 description of the preferred embodiments and to the drawings,
5 wherein:

6 FIG. 1 is a schematic drawing depicting a closed Brayton
7 cycle system; and

8 FIG. 2 is side sectional view of a direct contact
9 reactor/storage tank configuration according to the present
10 invention.

11 DESCRIPTION OF THE PREFERRED EMBODIMENT

12 Referring now to FIG. 1, there is shown a closed cycle
13 Brayton propulsion system 10 used to turn a drive shaft 12. A
14 compressor 14 driven by shaft 12 compresses a working gas. A
15 regenerator 16 for preheating the working gas is placed in
16 communication with the high pressure end of compressor 14. The
17 output of regenerator 16 is operatively connected to carry the
18 warmed gas to a reactor/storage tank 18 and an oxidant mixing
19 valve 20. An oxidant storage tank 22 controlled by an oxidant
20 control valve 24 is in communication with an injector 26 in
21 reactor/storage tank 18. Injector 26 injects an oxidant into the
22 reactor/storage tank where the oxidant reacts with the liquid
23 metal fuel to produce heat. Oxidant mixing valve 20 acts to mix
24 part of the warmed working gas with the oxidant to cool the
25 temperature at injector 26.

1 Reactor/storage tank 18 is partially filled with liquid
2 metal fuel. The warmed working gas enters reactor/storage tank
3 18 through working gas inlet tube 28 positioned below the surface
4 of the liquid metal fuel in reactor/storage tank 18. A working
5 gas outlet 30 is positioned in reactor/storage tank 18 above the
6 surface of the liquid metal fuel. A turbine 32 is connected with
7 working gas outlet 30 to receive the heated, high pressure,
8 working gas.

9 Turbine 32 expands the working gas and mechanically
10 transmits the extracted energy through drive shaft 12. Low
11 pressure working gas from turbine 32 is transferred to
12 regenerator 16 where the hot, low pressure working gas can
13 transfer its heat to the cool, high pressure working gas passing
14 from compressor 14 to reactor/storage tank 18. Low pressure gas
15 exits from regenerator 16 and passes to a cooler 34 where the
16 working gas is cooled by contact with the environment. In the
17 preferred embodiment seawater is used to cool the working gas.
18 Cool low pressure working gas is transported from cooler 34 to
19 compressor 14.

20 An accumulator 36 having an accumulator input valve 38 and
21 an accumulator output valve 40 is shown in communication between
22 the compressor 14 output and input. Accumulator 36 can be
23 initially filled with the working gas under pressure prior to
24 initiation of the cycle. At start up, accumulator output valve
25 40 is opened to allow the working gas to enter the system. At
26 any time during operation when the compressed working gas has

1 higher pressure than the gas in accumulator 36, the power to the
2 system can be reduced by opening accumulator input valve 38 and
3 withdrawing working gas from the system.

4 Compressor 14 is mechanically connected to receive power
5 from turbine 32 via drive shaft 12 mechanically connected to
6 turbine 32. A drive means or other power consuming device can
7 also be mechanically connected to receive power from drive
8 shaft 12.

9 Referring now to FIG. 2, there is shown a detail view of the
10 reactor/storage tank 18 of the current invention.

11 Reactor/storage tank 18 is a tank partially filled with liquid
12 metal fuel 42. Oxidant injector 26 and working gas inlet tube 28
13 are disposed below the surface of liquid metal fuel 42. Oxidant
14 injector 26 is preferably made from tungsten. Working gas inlet
15 tube 28 is a tube with a plurality of apertures 28a along the length
16 thereof to disperse the working gas evenly through liquid metal
17 fuel 42. Representative working gas bubbles 43 are shown leaving
18 aperture 28a and expanding toward the surface of liquid metal
19 fuel 42. Working gas outlet 30 is disposed above the surface of
20 liquid metal fuel 42. A filter 44 and a screen 46 are disposed
21 above the surface of fuel 42 between working gas outlet 30 and
22 the surface. Filter 44 and screen 46 cover the entire surface of
23 the fuel to prevent fuel and contaminants from entering working
24 gas outlet 30. Screen 46 is typically stainless steel or another
25 refractory metal. Filter 44 is typically a ceramic fiber
26 insulation filter.

1 The preferred fuel is an aluminum-magnesium alloy. The
2 oxidant in the preferred embodiment is O₂, and the preferred
3 working gas is a mixture of helium, and xenon. The mixture of
4 helium and xenon is preferred because of its heat transfer
5 characteristics; however, argon is frequently substituted for the
6 helium-xenon mixture for economic reasons. The working gas used
7 should have a molecular weight of 20 to 50 grams/mole and be
8 chemically inert with respect to the oxidant and fuel. The
9 selected percentage of helium, argon and xenon used is dependent
10 upon several factors including machinery size, pressure drop in
11 reactor/storage tank 18 versus heat transfer, and performance
12 capabilities of regenerator 16 and cooler 34.

13 The pressure of the inert gas mixture must be low enough to
14 allow sufficient dwell time for proper heat transfer and to
15 minimize splashing of liquid metal fuel 42 at its surface.

16 In operation, after the metal fuel is heated to the liquid
17 state, the working gas is ejected through working gas inlet 28
18 into reactor/storage tank 18 where the working gas bubbles
19 through liquid metal fuel 42. Thus, heat is transferred
20 directly from liquid metal fuel 42 to the working gas. The
21 liquid metal fuel 42 is maintained at a bulk temperature
22 slightly above the required turbine inlet temperature.

23 The oxidant is directly injected from oxidant tank 22 into
24 liquid metal fuel 42 through oxidant injector 26. The oxidant
25 is substantially consumed by reaction with liquid metal fuel 42,
26 and, thus, little of the oxidant will exit through working gas

1 outlet 30. The oxidant must be stored in oxidant tank 22 and
2 supplied at a high pressure since the oxidant will not pass
3 through compressor 14. The products of the reaction sink to the
4 bottom of reactor/storage tank 18 where they will not interfere
5 with combustion or the flow of working gas. Furthermore, the
6 products of the liquid metal/oxidant reaction must provide
7 substantially the same volume as the fuel alone.

8 Temperatures caused by the oxidizing reaction near injector
9 26 can be in excess of 8,000°F. To prevent excessive injector
10 wear, the oxidant can be mixed with a portion of the working gas
11 using oxidant mixing valve 20 before injection into
12 reactor/storage tank 18 to reduce the injection plume
13 temperature.

14 The advantages of the present invention are numerous.
15 Since the working gas and liquid metal fuel are inert with
16 respect to each other, direct contact heating is made possible.
17 Thus, heating efficiency is greatly increased over prior art
18 devices which utilize heat transfer tubes coiled within a
19 reactor. In addition, there is no danger of an explosive
20 reaction between the working gas and the liquid metal fuel.
21 Thus, the resulting closed Brayton cycle propulsion system is
22 safer for the environment than the currently used lithium/water
23 Rankine cycle system.

24 The working gas can be used to control the temperature of
25 the liquid metal fuel at the injector. By reducing temperatures
26 at the oxidizing agent injectors, the useful life of the system

1 is increased and system cost is decreased. In addition, all
2 noise associated with phase change is eliminated by using a
3 closed Brayton cycle.

4 The invention disclosed herein may be practiced other than
5 as specifically disclosed. For example, the accumulator can be
6 omitted, the regenerator and cooler may differ structurally from
7 those disclosed herein, and the inert gas/oxidant mixing system
8 can be omitted if the injector can withstand the reactor
9 temperatures.

10 Thus, it will be understood that many additional changes in
11 the details, materials, steps and arrangement of parts, which
12 have been herein described and illustrated in order to explain
13 the nature of the invention, may be made by those skilled in the
14 art within the principle and scope of the invention as expressed
15 in the appended claims.